

# STATISTICAL MOLECULAR THERMODYNAMICS

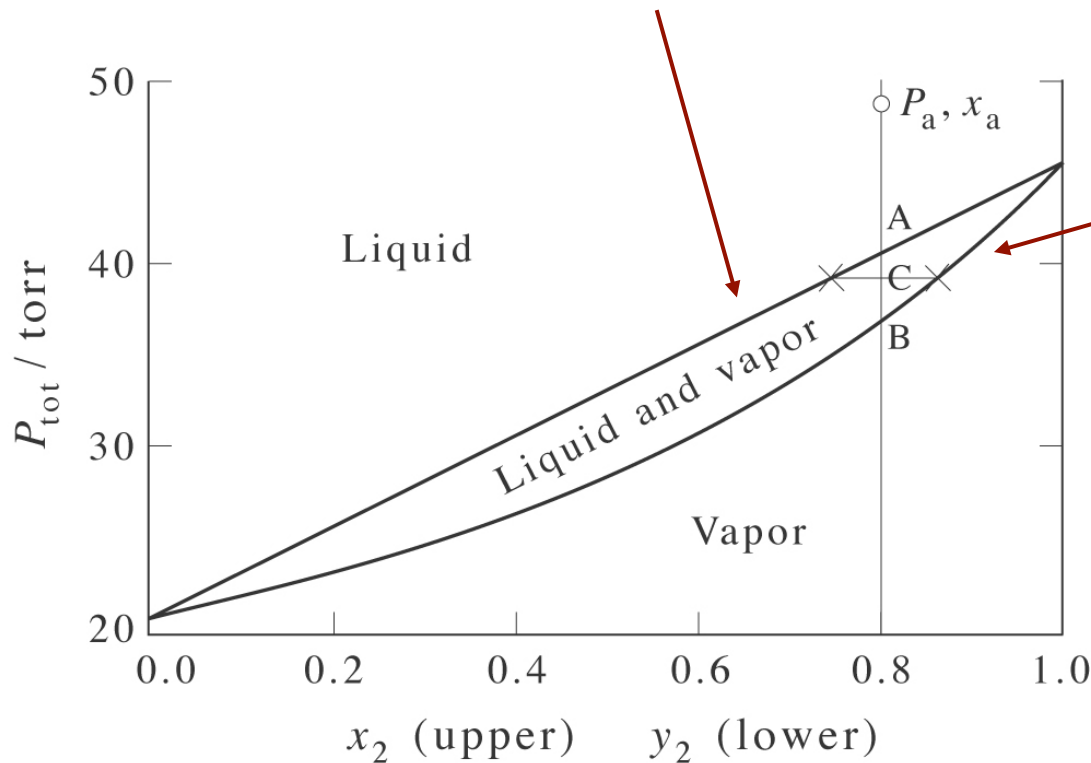
*Christopher J. Cramer*

Video 10.5

Ideal Solutions II

# SOLUTION LIQUID-VAPOR TRANSITIONS

Total VP as a function of the composition of the solution — linear for ideal solution — apply higher pressure, only liquid phase present



1-propanol/2-propanol at 25 °C

Pressure-composition diagram

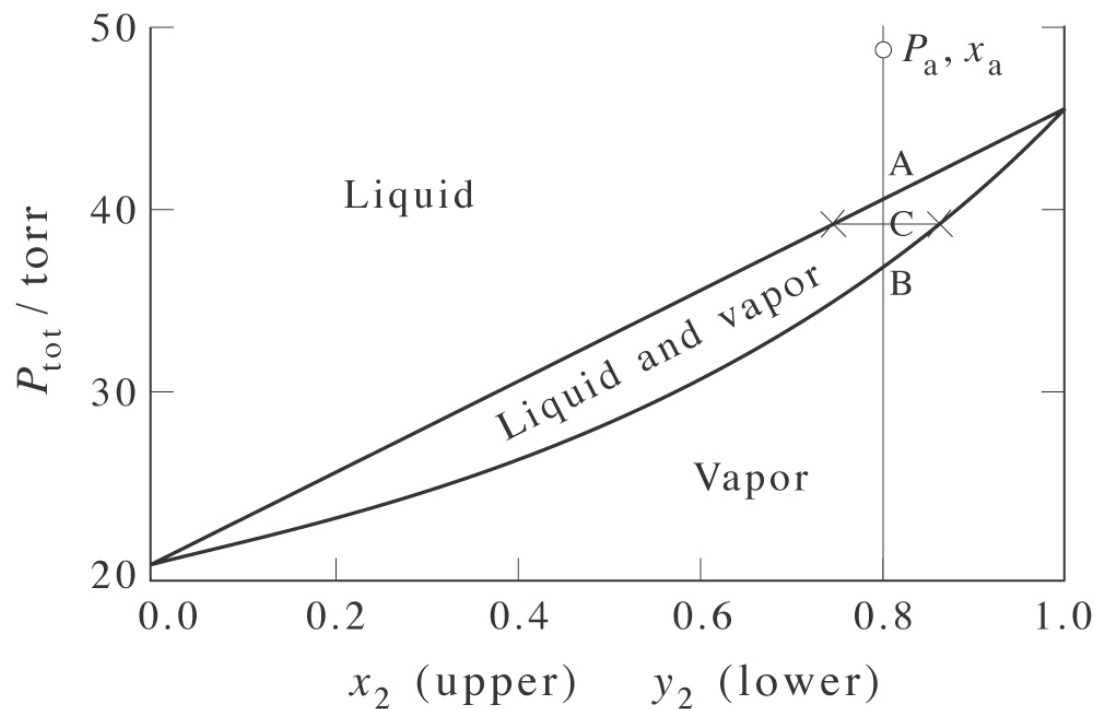
Total VP as a function of the composition of the vapor. From Laws of Dalton and Raoul:

$$y_2 = \frac{P_2}{P_{\text{total}}} = \frac{x_2 P_2^*}{P_{\text{total}}}$$

Of course, there's only a *single* pressure; the vapor is enriched in the lower boiling component compared to the higher until *all* is vapor at low  $P$

# Self-assessment

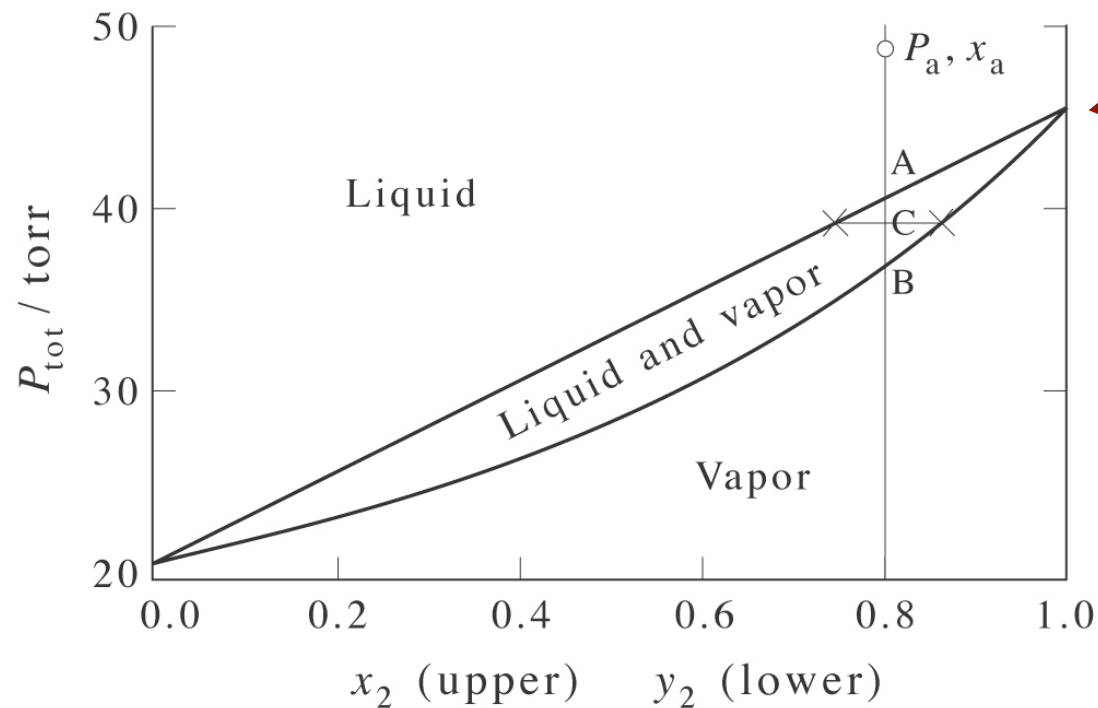
Explain the relationship between  $y_2$  and  $x_2$  in words, and especially, why is the former to the right of the latter given the dictates of Dalton's and Raoult's Laws?



$$y_2 = \frac{P_2}{P_{\text{total}}} = \frac{x_2 P_2^*}{P_{\text{total}}}$$

# Self-assessment Explained

$P_2^*$  must always exceed  $P_{\text{total}}$  unless the liquid is pure phase 2, so  $y_2$  will always be to the right of  $x_2$ . And, the ratio of  $P_2^*$  to  $P_{\text{total}}$  will be *greatest* when the solution is nearly pure component 1 (i.e.,  $P_{\text{total}}$  will be nearly  $P_1^*$ ). So, the  $y_2$  curve angles sharply away from the  $x_2$  curve at the outset, but ultimately rejoins it at the stage of pure liquid 2.



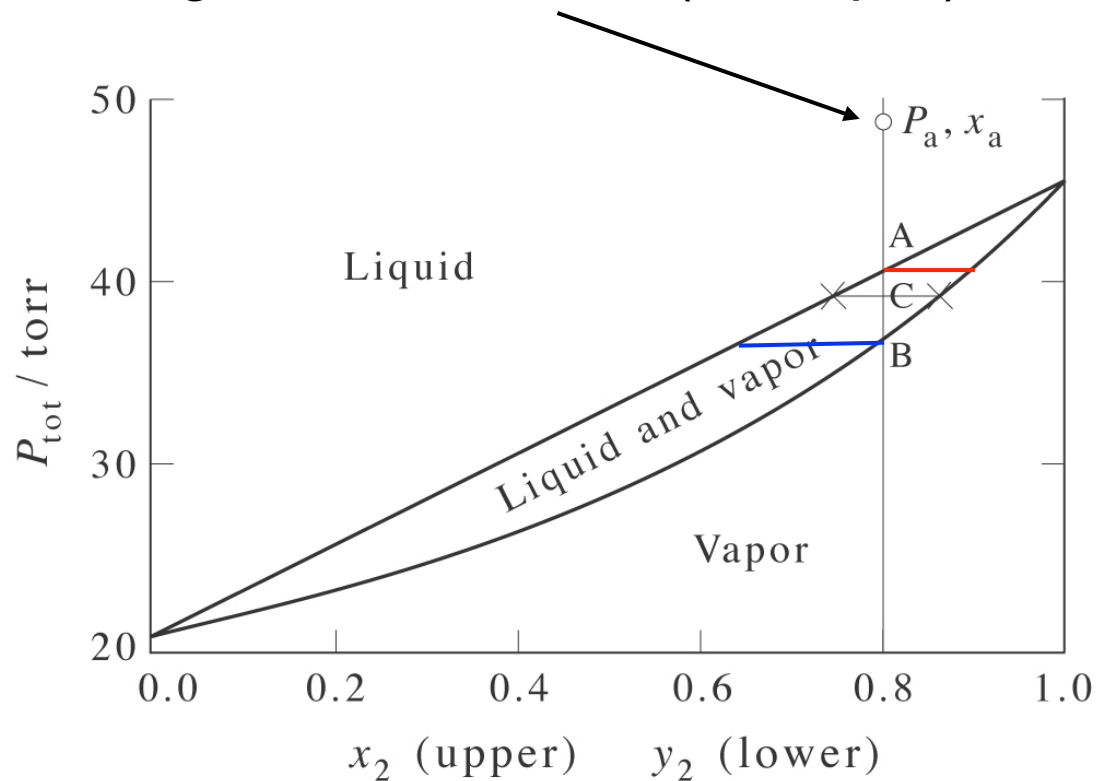
$$y_2 = \frac{P_2}{P_{\text{total}}} = \frac{x_2 P_2^*}{P_{\text{total}}}$$

*It's also helpful to think about case where  $x_1 = x_2 = 0.5$  and  $P_1^*$  vs  $P_2^*$  to understand how vapor is enriched in higher boiling component*

# VAPORIZING THE LIQUID SOLUTION

Consider a specific composition, 0.2:0.8 *n*-PrOH:*i*-PrOH

Begin at  $P = 50$  torr (no vapor), start pulling vacuum...



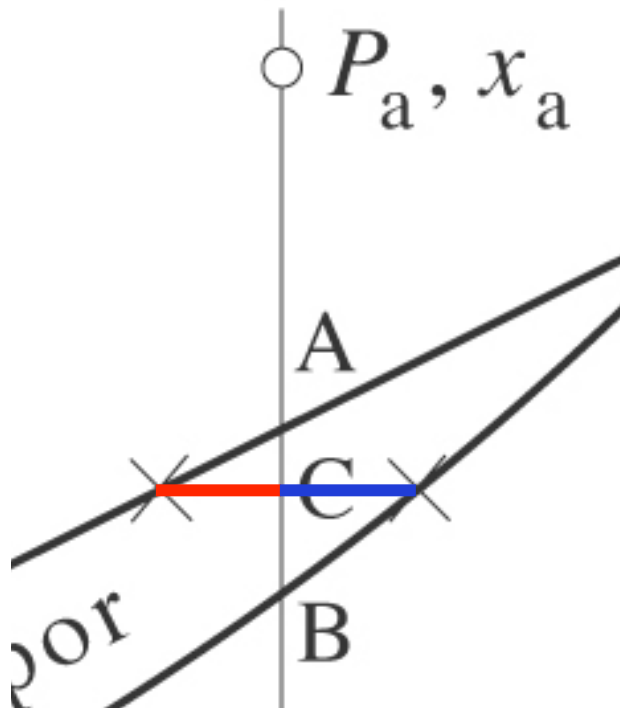
1-propanol/2-propanol at 25 °C

Pressure-composition diagram

At pressure A, the first vapor would begin to appear; it will be ~0.1:0.9 in composition, so the liquid perforce will begin to *decrease* in component 2

At pressure B, the last liquid to disappear will be ~0.35:0.65 in composition, and then the system will be *all* vapor with, of course, the original 0.2:0.8 composition

# ZOOMING IN ON THE TWO-PHASE REGION



Consider point C, which lies on a line connecting the composition of the liquid ( $x_2 = 0.75$ ) and vapor ( $y_2 = 0.87$ ). This line is called a tie-line. Remember that the overall *system* composition (i.e., liquid *and* vapor) is  $x_a = 0.80$

The total moles of liquid and of vapor can be determined from the *Lever Rule*

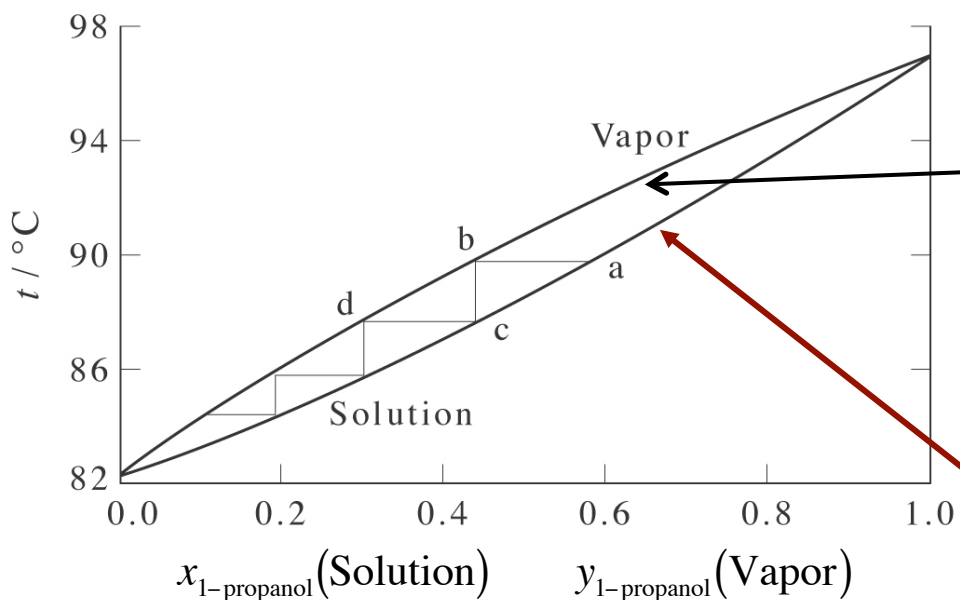
The *total* mole fraction that is liquid ( $x^l$ ):

$$\frac{n^l}{n^v} = \frac{y_2 - x_a}{x_a - x_2} = \frac{\text{blue}}{\text{red}}$$

$$x^l = \frac{\text{blue}}{\text{red} + \text{blue}}$$

# FRACTIONAL DISTILLATION

1-propanol/2-propanol at 760 torr



Using Dalton's/Raoult's laws:

$$y_1 = \frac{P_1}{760 \text{ torr}} = \frac{x_1 P_1^*}{760 \text{ torr}}$$

and:

$$P_{total} = 760 \text{ torr} = P_2^* - x_1(P_2^* - P_1^*)$$

bp as a function of composition

So, at 90 °C (between the two pure component boiling points) the composition of the liquid is 59 mol% 1-propanol (point a) and the vapor is 45 mol% 1-propanol (point b)

*Fractional distillation: vapor is condensed and revaporized many times a to b to c to d to ... and finally you get to the pure lower boiling component at the top (the coolest point) of a distillation head!*

$$dU = \delta q + \delta w$$



*Next: Non-ideal Solutions*