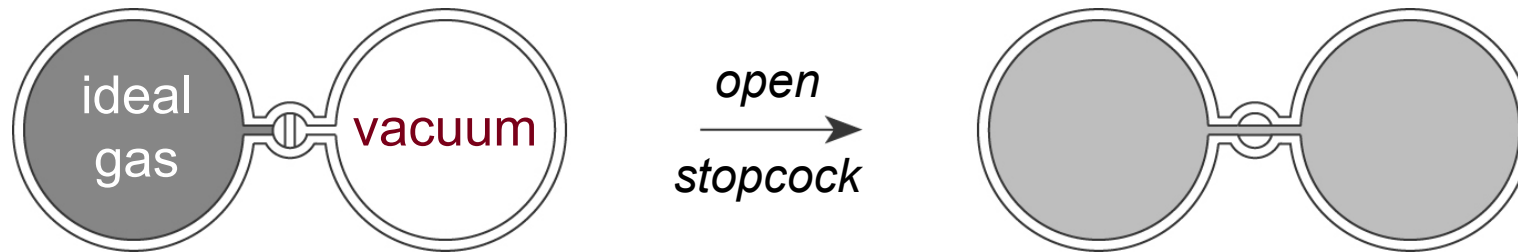


# USING STATE FUNCTION CHARACTER



This is *not* a reversible process! But, because entropy is a *state function*,  $\Delta S$  does *not* depend on the path.

Thus, we can use: 
$$\Delta S = \int_1^2 \frac{\delta q_{rev}}{T} \quad \delta q_{rev} = dU - \delta w_{rev}$$

$$dU = 0, \quad \delta q_{rev} = -\delta w_{rev}$$
  
*isothermal*

$$\Delta S = \int_1^2 \frac{\delta q_{rev}}{T} = -\int_1^2 \frac{\delta w_{rev}}{T}$$

$$\delta w_{rev} = -\frac{nRT}{V} dV \quad \leftarrow \text{reversible}$$

$$= nR \ln \frac{V_2}{V_1} > 0$$

# IRREVERSIBLE VS REVERSIBLE

The difference is the change in entropy of *the surroundings*

## Reversible case:

$$\Delta U = 0 \quad \leftarrow \text{isothermal}$$

The gas *absorbs heat from the surroundings*, so *the entropy of the surroundings decreases*.

$$q_{rev} = -w_{rev} = nRT \ln \frac{V_2}{V_1} \quad \Delta S_{surr} = -\frac{q_{rev}}{T} = -nR \ln \frac{V_2}{V_1}$$

$$\Delta S_{total} = S_{sys} + S_{surr} = 0$$

No change in *total* entropy, as expected for a reversible process

# IRREVERSIBLE VS REVERSIBLE

The difference is the change in entropy of *the surroundings*

**Irreversible case** (stopcock opened all at once):

$$\Delta U = 0$$

*isothermal*

No heat is transferred from the surroundings,  
so *the entropy of the surroundings is unchanged.*

$$P_{ext} = 0, \text{ so } w_{irr} = 0, \text{ so } q_{irr} = 0$$

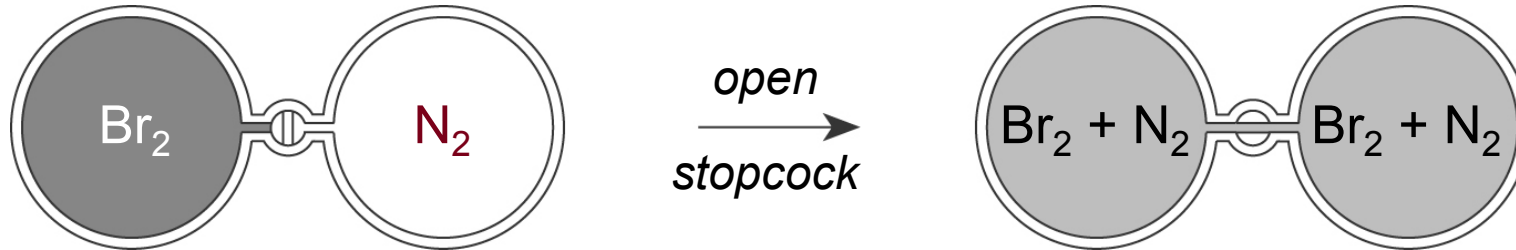
$$\Delta S_{surr} = 0$$

$$\Delta S_{total} = S_{sys} + S_{surr} = nR \ln \frac{V_2}{V_1} + 0 = nR \ln \frac{V_2}{V_1}$$

Total entropy *increases*, as expected for an irreversible process

*Technical note: we used the irreversible heat to compute the change in entropy of the surroundings. This is valid because there is zero work, so heat becomes a state function*

# ENTROPY OF MIXING



For each gas  $i$ ,

$$\Delta S_i = n_i R \ln \frac{\sum_j V_{j,0}}{V_{i,0}} = -n_i R \ln \frac{V_{i,0}}{\sum_j V_{j,0}}$$

where  $V_{j,0}$  is the original volume occupied by gas  $j$

But for ideal gases at the same  $T$ ,  $V$  is proportional to  $n$

$$\Delta S_i = -n_i R \ln \frac{n_i}{\sum_j n_j} \quad \Delta S_{\text{mix}} = -R \sum_i n_i \ln y_i \text{ where,}$$

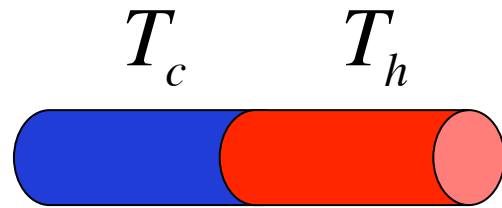
$$y_i = \frac{n_i}{\sum_j n_j}$$

*always greater than zero, so mixing is spontaneous*

*mole fraction*

# METAL BAR TEMPERATURE EQUILIBRATION

Heat transfer between two identical pieces of the same material



Since no work (negligible  $\Delta V$ ):

$$\delta q_{\text{rev}} = dU = dq = C_V dT$$

If  $C_V$  is independent of  $T$ :

$$\Delta q = C_V (T_f - T_i)$$

Heat lost equal/opposite to heat gained:

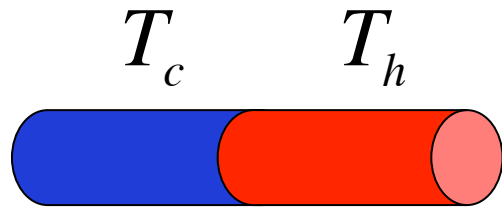
$$C_V (T_f - T_h) = -C_V (T_f - T_c)$$

$$\Rightarrow T_f = (T_c + T_h)/2$$

$$\Delta S = \int_{T_i}^{T_f} \frac{dq}{T} = C_V \int_{T_i}^{T_f} \frac{dT}{T} = C_V \ln\left(\frac{T_f}{T_i}\right)$$

# METAL BAR TEMPERATURE EQUILIBRATION

Heat transfer between two identical pieces of the same material



$$\Delta S = \int_{T_i}^{T_f} \frac{dq}{T} = C_V \int_{T_i}^{T_f} \frac{dT}{T} = C_V \ln\left(\frac{T_f}{T_i}\right)$$

The cold rod:

$$\Delta S = C_V \ln\left(\frac{T_c + T_h}{2T_c}\right)$$

The hot rod:

$$\Delta S = C_V \ln\left(\frac{T_c + T_h}{2T_h}\right)$$

Total: *Spontaneous?*

$$\Delta S = C_V \ln\left[\frac{(T_c + T_h)^2}{4T_c T_h}\right]$$

$$(T_c - T_h)^2 > 0$$

$$T_c^2 - 2T_c T_h + T_h^2 > 0$$

$$T_c^2 + 2T_c T_h + T_h^2 > 4T_c T_h$$

$$(T_c + T_h)^2 > 4T_c T_h \quad \checkmark$$